Amendments to the Claims:

This listing of claims will replace all prior versions, and listings of claims in the application:

Listing of Claims:

Please amend the claims as shown.

Claims 1-33. (Cancelled).

Claim 34. (Currently Amended) A process for preparing a shell-type catalyst comprising:

a) applying a suspension to a substantially nonporous inorganic support material having a BET surface area of less than $80 \text{ m}^2/\text{g}$ and a diameter of 0.5 mm to 50 mm, the suspension consisting

essentially of:

(i) at least one water soluble catalytically active metal compound; and

(ii) a substantially water insoluble coating compound selected from the group consisting of:

SiO₂, Al₂O₃, TiO₂ and ZrO₂;

b) drying said suspension onto said support material; and

c) activating in a reducing gas stream.

Claim 35. (Previously Presented) The process according to claim 34, wherein said suspension

consists of said water soluble metal compound and said substantially water insoluble coating

compound selected from the group consisting of: SiO₂, Al₂O₃, TiO₂ and ZrO₂.

Claim 36. (Previously Presented) The process according to claim 34 or 35, wherein said

support material comprises a granulate or molded article of at least one member selected from

the group consisting of glass, quartz, ceramic, silica, alumina, graphite, molded carbon, metal

and steatite.

Claim 37. (Previously Presented) The process according to claim 34 or 35, wherein said support material comprises a molded article of at least one member selected from the group consisting of SiO₂ and Al₂O₃.

Claim 38. (Previously Presented) The process according to claim 36, wherein said molded article comprises at least one member selected from the group consisting of a hollow extrudate, solid extrudate, sphere, granule, tablet and strand.

Claim 39. (Cancelled)

Claim 40. (Previously Presented) The process according to claim 34 or 35, wherein the BET surface of said support material is less than 10 m²/g.

Claim 41. (Previously Presented) The process according to claim 34 or 35, wherein said substantially nonporous support material has a pore volume of less than 0.5 ml/g.

Claim 42. (Previously Presented) The process according to claim 34 or 35, wherein said substantially nonporous support material has a pore volume of less than 0.1 ml/g.

Claim 43. (Previously Presented) The process according to claim 34 or 35, wherein said support material has an Fe₂O₃ content of less than 0.5% wt.

Claim 44. (Previously Presented) The process according to claim 34 or 35, wherein said water soluble catalytically active metal compound is a water soluble noble metal compound selected from the group consisting of Ru, Rh, Pd, Ag, Os, Ir, Pt and Au.

Claim 45. (Previously Presented) The process according to claim 44, wherein said water soluble metal compound is in the form of an oxide, hydroxide, carbonate, halide, nitrate, salt of an organic acid or a complex.

Claim 46. (Previously Presented) The process according to claim 44, wherein said suspension contains greater than 1% wt. aqueous solution of said water soluble noble metal compound calculated as the metal.

Claim 47. (Currently Amended) The process according to claim 44, wherein said suspension contains >5% wt. aqueous solution of said water soluble noble metal compound, calculated as the metal.

Claim 48. (Currently Amended) The process according to claim 44, wherein at least 0.01% wt. of said noble metal compound, calculated as the metal, is soluble in water at 30°C.

Claim 49. (Currently Amended) The process according to claim 34 or 35, wherein the maximum average agglomerate size of said oxide substantially water insoluble coating compound is 15 µm.

Claim 50. (Currently Amended) The process according to claim 34 or 35, wherein the agglomerate size of said exide substantially water insoluble coating compound is 3 µm to 7 µm.

Claim 51. (Previously Presented) The process according to claim 34 or 35, wherein the BET surface area of said water insoluble coating compound is from 50 m²/g to 500 m²/g.

Claim 52. (Previously Presented) The process according to claim 34 or 35, wherein the compacted density of said insoluble coating compound is from 10 g/l to 800 g/l.

Claim 53. (Previously Presented) The process according to claim 34 or 35, wherein the weight ratio of said water soluble noble metal compound to said insoluble coating compound calculated as the metal is from 0.1:1 to 5:1.

Claim 54. (Previously Presented) The process according to claim 53, wherein the weight ratio of said noble metal compound to said insoluble coating compound is between 0.5:1 and 2:1.

Claim 55. (Previously Presented) The process according to claim 34 or 35, wherein the weight ratio of said noble metal compound, calculated as the metal, to the total weight of the shell-type catalyst is between 0.0001:1 and 0.02:1.

Claim 56. (Previously Presented) The process according to claim 34 or 35, wherein the weight ratio of the coating compound to the total weight of the shell-type catalyst, calculated as the metal, is between 0.005:1 and 0.04:1.

Claim 57. (Previously Presented) The process according to claim 34 or 35, wherein the thickness of the coating shell of the catalyst is from 0.1 µm to 20 µm.

Claim 58. (Previously Presented) The process according to claim 34 or 35, wherein the concentration of the water soluble metal component, calculated as the metal, is from 0.1% wt. to 1% wt. based on the catalyst.

Claim 59. (Previously Presented) The process according to claim 34 or 35, wherein the concentration of the water insoluble coating material, calculated as the metal, is from 0.05% wt. to 1% wt. based on the catalyst.

Claim 60. (Previously Presented) The process according to claim 34 or 35, wherein said reducing gas stream contains hydrogen.

Claim 61. (Previously Presented) The shell catalyst produced by the process according to claim 34.